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Europäisches Patentamt
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11 Publication number:

0 446 616 B1

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EUROPEAN PATENT SPECIFICATION

45 Date of publication of patent specification: **07.12.94** 51 Int. Cl.⁵: **E21B 41/02, //C23F11/14**

21 Application number: **91101772.1**

22 Date of filing: **08.02.91**

The file contains technical information submitted
after the application was filed and not included in
this specification

54 **Process for inhibiting corrosion in oil production fluids.**

30 Priority: **09.02.90 DE 4003893**

43 Date of publication of application:
18.09.91 Bulletin 91/38

45 Publication of the grant of the patent:
07.12.94 Bulletin 94/49

64 Designated Contracting States:
AT BE CH DE DK ES FR GB GR IT LI LU NL SE

66 References cited:
DD-A- 234 897
FR-A- 1 451 354
GB-A- 1 062 359
US-A- 3 054 750
US-A- 4 201 678

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EP 0 446 616 B1

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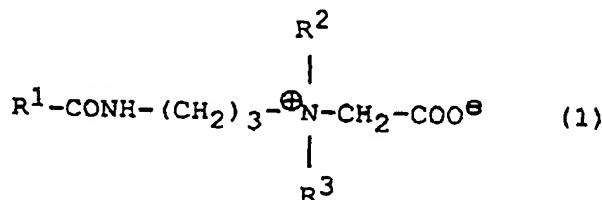
Description

Corrosion inhibitors used in oil production offshore are highly cationic but the use of such cationic based corrosion inhibitors for offshore oil platforms are becoming less acceptable for environmental reasons. By being cationic they are attracted to metal surfaces, controlling acid type corrosion. When these cationic corrosion inhibitors find their way into the seawater, they are attracted to a particular type of algae, diatoms. These algae are a part of a food-chain for mussels.

It has been reported that a corrosion inhibitor has not been found, that does not inhibit growth of these algae, at a concentration greater than 1 ppm. The diatoms have a skeleton structure of about 80 % silicon dioxide or quartz. Cationic materials, which make up most corrosion inhibitors are attracted to quartz as readily as they are to metals. Cationics used for producing corrosion inhibitors, can be quaternary amines, amine salts, ethoxylated amines, ether amines, polyamines, amido amines, essentially all nitrogen based molecules are candidates for producing corrosion inhibitors.

US-A-3,054 750 discloses the use of compounds according to formula $\text{CH}_3\text{H}_2\text{CH}_2\text{NHCH}_2\text{CH}_2\text{COOH}$ as corrosion inhibitors in oil well fluids. Amounts of inhibitor in the oil well fluid are within the range of 50 to 400 ppm.

US-A-4,201,678 discloses the use as foaming agent of amphoteric betaine of the formula

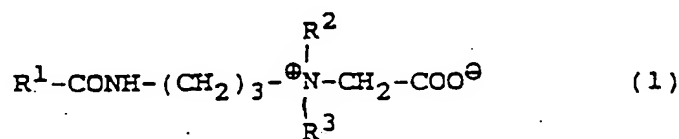


in combination with a sodium olefin sulfonate in an oil production fluid (drilling fluid). The amount of such additive in the drilling fluid is ranging from 0.08 to 1.0 wt% (800 to 10.000 ppm).

Due to the decreased toxic properties and the ampholytic characteristics of the ampholytes and betaines, the biodegradability is greatly increased. Thereby reducing the possibility of these products ever reaching toxic levels.

It has now been found that this problem can be overcome by using certain betaines or ampholytes as corrosion inhibitors.

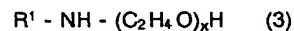
Accordingly the subject matter of the instant invention is a process for inhibiting corrosion in oil production fluids which process consists in adding to the oil production fluids under acidic conditions an effective amount of a betaine or ampholyte of the formula 1



wherein R^1 is C_{10} - C_{20} -alkyl or C_{10} - C_{20} -alkenyl, preferably C_{14} - C_{18} -alkyl or C_{14} - C_{18} -alkenyl and R^2 and R^3 are C_1 - C_4 -alkyl, preferably methyl.

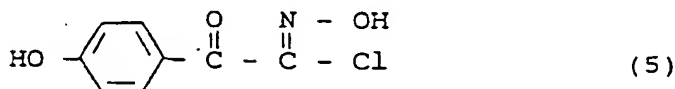
These betaines and ampholytes as described before can be used as such or they can be used upon being neutralized with acids such as, but not limited to acetic acid, adipic acid, sebacic acid, naphthenic acids, paraffinic acids, tall oil acids or free SO_2 . They function as corrosion inhibitors in oil production fluids containing acid such as carbon dioxide as corrodent. Carbon dioxide is the most common acid in oil production fluids.

In addition these betaines and ampholytes can also be used together with other corrosion inhibitors to reduce the toxicity, preferably oxalkylated fatty amines of the formulas 3 or 4





wherein R^1 is as defined above and x is a number from 5 to 15 or a compound of the formula 5



The betaine or ampholyte compound of formula 1 or the mixtures of these compounds with the compounds of formulas 3, 4 and/or 5 are added to the oil production fluids at a rate that is effective to prevent corrosion. Under usual conditions an amount of 5 to 300, preferably 2 to 20 ppm will be sufficient.

When the betaines or ampholytes of formula 1 are dumped to neutral or alkaline pH-water, such as seawater, they lose their cationic characteristics, and take on the characteristics of nonionic or anionic molecules. Under these conditions, they no longer function as corrosion inhibitors and they also will not inhibit the growth of the diatoms, as would be the case if they maintained their cationic characteristics.

Also the oxalkylated amines of formulas 3 and 4 do not function as cationics and therefore they lose their ability to be readily absorbed by the silicate in the diatoms. The same is with the p-hydroxy-benzoic acid derivative of formula 5 which hydrolyses at a pH greater than 7.5 forming non-toxic benzoates.

Formulations for use on the basis of the above described betaines and their mixtures with compounds of formulas 3, 4 and/or 5 can be made by dissolving these compounds in a mixture of water and lower alcohols.

Example 1

12 % tallow fatty acid-amidopropyl-N,N-dimethyl-N-carboximethyl-betaine
5 % adipic acid
10 % isobutanol
5 % methanol
water ad 100 %

Example 2

12 % tallow fatty acid-amidopropyl-N,N-dimethyl-N-carboximethyl-betaine
3 % SO_2
10 % isobutanol
5 % methanol
water ad 100 %

Example 3

8 % tallow fatty acid-amidopropyl-N,N-dimethyl-N-carboximethyl-betaine
10 % isobutanol
5 % methanol
15 % mixture of alkyl pyridines
5 % SO_2
water ad 100 %

Example 4

10 % tallow fatty acid-amidopropyl-N,N-dimethyl-N-carboximethyl-betaine
5 % cocosdiamine + 15 moles ethylene oxide
10 % isobutanol
5 % methanol
water ad 100 %

Example 5

10 % tallow fatty acid-amidopropyl-N,N-dimethyl-N-carboximethyl-betaine

5 % compound of formula 5

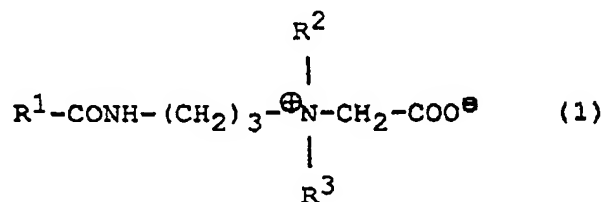
85 % mixture of propylene glycol and isobutanol

In the examples described before all percentages are by weight.

These compositions have been checked in a standard corrosion inhibitor test, referred to as a bubble test. In the presence of 80 % brine and 20 % crude oil, saturated with carbon dioxide, in a 24 hour test gave greater than 90 % protection, when measured by Corrator, at a treatment rate of 20 ppm. The same products in a dynamic autoclave test with 3 % sodium chloride, 10 bars of carbon dioxide pressure, 12 °C, containing 8 steel coupons, rotating at about 3 meter per second gave 60 % protection. There are a number of commercial inhibitors on the market, that give 40 % or less protection, others give greater than 90 % protection. Therefore, the compositions as described above are within the range of commercial corrosion inhibitors. These compositions have also been tested for growth inhibition of *Skeletonrema Costatum*, a standard toxicity test for marine diatoms, at a treating rate of 4 ppm and there was no apparent retardation of growth of the *Skeletonrema Costatum* up to 4 ppm and some at 8 ppm.

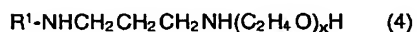
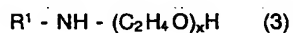
Claims

1. A process for inhibiting corrosion in oil production fluids which process consists in adding to the oil production fluids under acidic conditions an effective amount of a betaine or ampholyte of the formula (1)

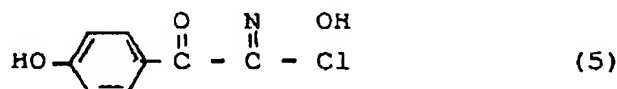


wherein R¹ is C₁₀-C₂₀-alkyl or C₁₀-C₂₀-alkenyl and R² and R³ are C₁-C₄-alkyl.

2. A process as claimed in claim 1, wherein R¹ is C₁₄-C₁₈-alkyl or C₁₄-C₁₈-alkenyl and R² og R³ are methyl.
3. A process as claimed in claim 1 or 2 which consists in adding 5 to 300, preferably 2 to 20 ppm of the betaine or ampholyte of formula (1) to the oil production fluids.
4. A process as claimed in any of claims 1-3 which consists in using the betaine or ampholyte of formula (1) together with oxalkylated fatty amines of formulas (3) or (4)

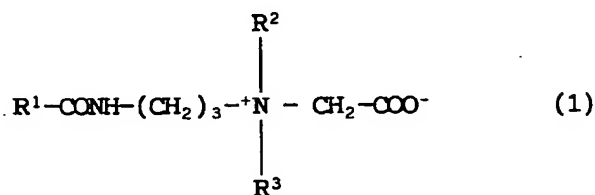


wherein R¹ is as defined for formula 1 and x is a number from 5 to 15, and/or a compound for the formula (5)



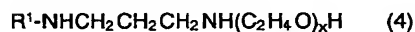
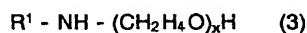
Patentansprüche

1. Verfahren zur Korrosionshemmung in Erdölförderflüssigkeiten, welches darin besteht, daß den Erdölförderflüssigkeiten unter sauren Bedingungen eine wirksame Menge eines Betains oder eines Ampholyten der allgemeinen Formel (1) zugesetzt wird:

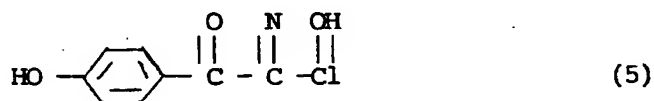


wobei R¹ ein Alkyl oder Alkenyl mit 10 bis 20 Kohlenstoffatomen und R² und R³ jeweils ein Alkyl mit 1 bis vier Kohlenstoffatomen sind.

2. Verfahren nach Anspruch 1, bei welchem R¹ ein Alkyl oder ein Alkenyl mit 14 bis 18 Kohlenstoffatomen und R² und R³ Methyl sind.
3. Verfahren nach Anspruch 1 oder 2, welches darin besteht, den Erdölförderflüssigkeiten 5 bis 300, vorzugsweise 2 bis 20 ppm Betain oder den Ampholyten der allgemeinen Formel (1) zuzusetzen.
4. Verfahren nach einem der Ansprüche 1 bis 3, welches darin besteht, das Betain bzw. den Ampholyten der allgemeinen Formel (1) zusammen mit oxalkylierten Fettaminen der allgemeinen Formel (3) bzw. (4)



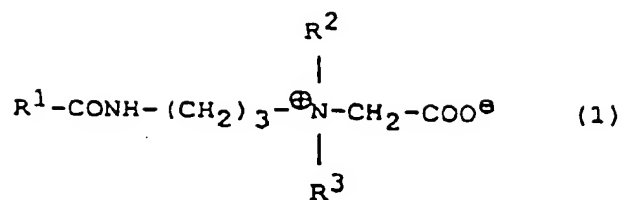
wobei R¹ die für die allgemeine Formel (1) angegebene Bedeutung hat und x eine Zahl zwischen 5 und 15 ist, und/oder eine Verbindung der allgemeinen Formel (5):



einzusetzen.

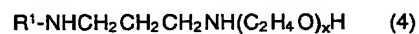
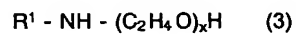
Revendications

1. Procédé pour inhiber la corrosion dans les fluides de production de pétrole, qui consiste à ajouter aux fluides de production de pétrole, en milieu acide, une quantité efficace d'une bétaine ou un ampholyte répondant à la formule (1) :



dans laquelle R¹ est un groupe alkyle en C₁₀ à C₂₀ ou alcényle en C₁₀ à C₂₀, et R² et R³ sont des groupes alkyle en C₁ à C₄.

2. Procédé selon la revendication 1, dans lequel R¹ est un groupe alkyle en C₁₄ à C₁₈ ou alcényle en C₁₄ à C₁₈, et R² et R³ sont des groupes méthyle.
3. Procédé selon les revendications 1 ou 2, qui consiste à ajouter 5 à 300, de préférence 2 à 20 ppm de la bétaine ou de l'ampholyte répondant à la formule 1 aux fluides de production de pétrole.
4. Procédé selon l'une quelconque des revendications 1 à 3, qui consiste à utiliser la bétaine ou l'ampholyte répondant à la formule (1) en même temps que des amines grasses oxalkylées répondant aux formules (3) ou (4)



dans lesquelles R¹ est tel que défini pour la formule 1 et x est un nombre de 5 à 15, et/ou un composé répondant à la formule (5)

